TOWARDS PREPARATION CONDITIONS FOR THE SYNTHESIS OF 1 ALKALI-ACTIVATED BINDERS USING TUNGSTEN MINING WASTE 2

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#### 11 ABSTRACT

12 This study evaluated the results of preparation conditions for the production of an alkali-13 activated binder (AAB) based on a binary mixture of tailings from tungsten mine waste 14 (TMW), and waste glass (WG) activated with a mixture of sodium silicate (SS) and sodium hydroxide (SH). 40 wt.% WG increased the amorphous nature of the binary blend by 21% 15 16 without initiating the alkali-silica reaction. SS/SH activator solution was subjected to a 17 variation of mixing times, and its sensitivity was measured using temperature monitoring, and 18 Fourier Transforms Infrared Spectroscopy (FTIR). After 20 minutes of mixing, the SS/SH 19 activator solution showed a 3.13°C reduction in temperature, a 21.4% increase in unbound 20 water content and as a result imparted a 26% drop in the mechanical resistance of TMW-WG 21 AAB at 28-days. The TMW-WG AAB was also determined to develop the highest compressive strength when cured at 80°C for 24h in sealed conditions. The following 22 23 conditions, supported by X-ray diffraction (XRD) and Fourier transforms infrared analysis 24 (FTIR), are responsible for the most significant dissolution of the alumino-silicate oxides.

Author keywords: alkali-activated binder; binary blend; curing temperature; geopolymer;
 material preparation; mixing time; precursor reactivity; synthesis conditions; tungsten mining
 waste; waste glass

### 28 INTRODUCTION

29

30 Although the development of Portland cement (PC) research and its application has 31 considerably matured in last few decades, it is still facing challenges due to its impact on the 32 environment. The production of cement is one of the industry's most energy intensive 33 processes next only to steel and aluminium (Napp et al. 2014). In 2011, the European states 34 accounted for 7.6% of total global cement production (European Cement Association 2014). 35 The manufacture of PC can consume approximately 3.2-6.3 GJ of energy (thermal and 36 electrical) per tonne of clinker product (Rahman et al. 2016) with almost half of this being 37 used for the fine grinding of clinker to make the cement. The main raw material used in 38 cement production has traditionally been the abundantly available limestone which, by its 39 inevitable transformation into lime, is responsible for over 60% of the cement industry's CO<sub>2</sub> 40 emissions (Mikulčić et al. 2012). For every kg of PC clinker produced, about 0.87 kg of CO<sub>2</sub> 41 is released (Telesca et al. 2017). Therefore, the main challenge of the cement industry is 42 focused on the CO<sub>2</sub> emission reduction to 1.55 Gt per year (about 45% of the current value) by 2050 (Telesca et al. 2017). 43

To reduce the carbon footprint and conveniently dispose of the variety of waste material available from multiple industries, alkali-activated binders (AABs for short hereafter) have attracted increasingly more attention from the scientific community as environmentally favourable alternatives to PC (Barbosa et al. 2000; Bădănoiu et al. 2015). Aluminosilicate rich materials can be chemically activated to produce a three-dimensional polymer like network containing both crystalline and amorphous phases (Davidovits 1981). These particular binders yield high strength with rapid setting, good durability and high resistance to chemical attack (Hardjito et al. 2009; Ariffin et al. 2013; Thomas and Peethamparan 2015). Despite the existence of strong economic and environmental drivers, alkali-activated binders are still not widely implemented throughout the world. They represent an attractive alternative for the partial or complete substitution of PC, offering comparable performance (Neupane 2016) and cost (Duxson et al. 2007a) while reducing greenhouse gas emissions (Duxson et al. 2007b).

57 The raw materials used for synthesising AABs are typically calcined clays or low-calcium fly 58 ashes (Duxson et al. 2007a). However, the supply of fly ash in Europe is in decline due to the 59 industry becoming increasingly less reliant on coal-fired power stations (Carroll 2015) while 60 the disposal of the 85% of host rock generated from kaolin clay mining is an increasingly 61 critical issue (Murray 2002). On the other hand, mining and quarrying waste still represent 62 15% of the total waste in Western Europe and 31% in Eastern Europe (Pacheco-Torgal et al. 63 2009b), while the USA alone is estimated to produce between 1000-2000 Mt of mining waste 64 annually (Szczepańska and Twardowska 2004). The favourable mineralogical composition of 65 mining waste for alkali activation (Jiao et al. 2013; Ye et al. 2014; Zhang 2014) combined with its continuously large production make it an attractive and environmentally friendly 66 67 feedstock for AABs.

Some mining and quarrying wastes can be reused in earthworks and construction, in particular, the coarser fractions. Typical applications include use in asphalt pavements (Albuquerque et al. 2006; Akbulut and Gürer 2007) and concrete (Yellishetty et al. 2008; Hebhoub et al. 2011). However, recent studies on the reuse of fine tailings as raw material for AABs are considered to be most promising; from an environmental, technical and economic point of views. For this study, the wastes of particular interest are fine tailings derived from tungsten mining. Preliminary research has been conducted on the transformation of this type 75 of waste into AABs and has shown promising results. Pacheco-Torgal et al. (2007) first 76 highlighted the potential of using calcined tungsten mining waste mud blended with calcium 77 hydroxide for the development of a high early strength geopolymeric binder. Tungsten 78 mining waste also identified to be very effective for stabilizing/solidifying heavy metals 79 particularly when used in conjunction with blast-furnace slag (Choi et al. 2009) and overall, 80 suggested that mortar with acceptable properties can be developed using up to 10% by mass 81 tungsten mining waste. Later, alkali-activated artificial aggregates were produced from such 82 mining waste mud, and their properties were studied as a potential substrate for fixed-film 83 wastewater treatment processes (biofilm reactors). The results showed that the aggregates 84 obtained have suitable resistance to acid attack and may be used as a substrate for fixed-film 85 biological reactors for the treatment of acid wastewaters (Silva et al. 2012a). Also, mine 86 tailings blended with other industrial by-products such as fly ash have resulted in the 87 production of an AAB with high compressive strength, mainly due to the Si/Al ratio of the 88 raw material blend falling within the optimum Si/Al ratio for alkali-activation (Zhang et al. 89 2011; Ahmari and Zhang 2012).

90 Despite the research conducted so far, it remains that tungsten mining waste possesses a low 91 degree of reactivity due to it crystalline phases. Thermal treatments have previously been 92 studied to improve the amorphicity of tungsten mining waste, and satisfactory strengths have 93 been achieved (Pacheco-Torgal et al. 2009b), nonetheless at the expense of the high amount 94 of energy. A more sustainable method would be to blend the tungsten mining waste with a 95 material that would increase not only its level of amorphicity but also maintain its 96 environmental appeal. In this case, waste glass would be the ideal candidate since it is a very 97 common construction and household waste material with a highly amorphous structure. It is estimated that out of 18 million tonnes of glass wastes accumulated in 2012 in the EU, only 98 99 35% of this was recycled (Glass for Europe 2013). The feasibility of using ground waste

glass to improve mechanical performance has already been achieved with PC concrete (Shao
et al. 2000a) and initiated with metakaolin based AABs (Christiansen and Sutter 2013).

102 Also when assessing novel binder materials, it is of as much importance to study the 103 preparation/manufacturing techniques as it is the final material properties. This is a domain 104 which currently remains understudied for AABs in general, let alone those based on tungsten 105 mining waste.

Thus, the primary objective of this study is to determine the fundamental aspects of AAB synthesis using tungsten mining waste as the principle raw material with the added feasibility of its partial replacement by waste glass. Particular focus will be on (1) the influence of waste glass on tungsten mining waste reactivity; (2) alkali activator solution preparation and kinetics; (3) AAB curing temperature and curing duration.

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## 112 MATERIALS AND METHODS

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#### 114 Materials

The raw materials used in this investigation consisted of tungsten mining waste (TMW), 115 116 waste glass (WG), sodium hydroxide (NaOH) (SH), and sodium silicate (Na<sub>2</sub>SiO<sub>3</sub>) (SS). The 117 TMW was derived in powder form from the Panasqueira mine in Castelo Branco, Portugal, 118 and the WG was received from the local municipality of Covilhã, Portugal. The chemical 119 composition of the TMW and WG as obtained by SEM-EDX (SUPRA 35VP/EDAX). Due to 120 the waste nature and microscopic inhomogeneity of the TMW, chemical analyses were made 121 from different batches collected from the mine. Therefore, the results of TMW reported in 122 Table 1 are the average values accompanied with the standard deviation (S.D). According to 123 Table 1, for TMW, the oxides SiO<sub>2</sub>, Al<sub>2</sub>O<sub>3</sub>, Fe<sub>2</sub>O3, and SO<sub>3</sub> are the most abundant, while the 124 oxides SiO<sub>2</sub>, MgO, SO<sub>3</sub> and Fe<sub>2</sub>O<sub>3</sub> showed the greatest variability. Grain size distribution analysis was performed for the precursor materials after mechanical sieving by laser 125

126 diffraction analysis according to BS ISO 13320:2009. The TMW has a mean particle size of 127 26µm while the waste glass has a mean particle size of 39.6µm. The WG was intentionally 128 used with a slightly larger mean particle size to reduce the energy consumption during the 129 milling process. The bulk powder densities of TMW and WG were determined using a gas displacement pycnometer (AccuPyc II 1340) and were determined as 3.08 and 2.53 g/cm<sup>3</sup>, 130 131 respectively. Sodium hydroxide solution was prepared by dissolving sodium hydroxide pellets (98% purity obtained from Fisher Scientific) in de-ionized water and allowed to cool 132 133 before use. Sodium silicate (obtained from Solvay SA, Portugal) had a  $SiO_2/Na_2O = 3.23$ 134 (8.60 wt.% Na<sub>2</sub>O, 27.79 wt.% SiO<sub>2</sub>, 63.19wt.% H<sub>2</sub>O, 0.4wt.% Al<sub>2</sub>O<sub>3</sub>).

135 Synthesis of samples

All experiments were carried out at 20°C. TMW alkali-activated binders with up to 40 mass-% replacement with WG were blended with an IKA Ultra-Turrax T50 mixer at 360 rpm for 60 s. Based on the research on alkali-activation available in the literature concerning mechanical strength and efflorescence formation potential in AABs combined with the experience gained from previous studies (Pacheco-Torgal et al. 2008; Silva et al. 2012b; Kastiukas et al. 2016), the following ranges were selected for the constituents of the AABs:

- Molarity of SH = 10M
- Weight ratio of SS/SH = 4

## • Weight ratio of precursor/activator = 3.6

The following ratios produced an AAB with a flowability of  $130 \pm 5$ mm determined using the method proposed by EN 1015-3:1999 (2006) and initial and final setting times of 90 and 110 minutes determined EN 196-3 (European Committee for Standardization 2005). In the precursor/activator ratio, the precursor is the TMW and WG, and the activator is the solution containing the alkali, the silicate and the water. 150 To produce the TMW-WG AAB, the TMW, and WG were mixed in the dry state for five minutes, forming the precursor materials. The sodium hydroxide and sodium silicate 151 152 solutions were mixed for a period ranging from 2.5 to 60 mins at 700 rpm, depending on the 153 type of condition being tested, forming the alkali activator. The alkali-activator solution was slowly added to the precursor materials, and the resulting paste was stirred for 2.5 minutes at 154 155 200 rpm, followed by 2.5 minutes at 400 rpm. The resulting AAB was then placed in 40x40x160 mm<sup>3</sup> prismatic Styrofoam moulds. The mould was filled with the AAB in three 156 157 stages and manually vibrated after each successive filling stage to release trapped air bubbles, 158 and sealed with a film to avoid the loss of water and ingress of CO<sub>2</sub>. Samples which were 159 made to test curing exposed to the atmosphere were cured unsealed. The specimens were 160 placed in a temperature and humidity controlled environmental chamber at 50% RH for 161 curing between 20 and 80°C for 4-36h, depending on the type of condition being tested. After curing, prisms were de-moulded and left in a laboratory condition of 20°C for curing 162 163 until the test age. The specimens cured at 20°C were de-moulded after 48 h due to a slow 164 setting. Table 2 summarises synthesis conditions tested in this study i.e. activator solution mixing time, curing temperature and curing time. 165

166 To observe for chemical changes in the activator solution during mixing, the first it was decided to isolate the activating solution and monitor its temperature during the mixing 167 168 process. The temperature evolution of the activator solution was measured using the setup 169 shown in Fig. 1. The activator solution was prepared at the same SS/SH solution ratio as that 170 used to make the TMW-WG ABB i.e. 4.0. A polystyrene enclosure was used to contain the 171 activator solution and provided a thermodynamically stable environment. Two K-type 172 thermocouples with the tips wrapped in temperature sensitive copper tape were connected to 173 a multi-channel data logger and used to measure the temperature of the activator solution and enclosure's interior, respectively. Once the activator temperature was deemed constant,mixing was started and continued for 20 minutes at 700 rpm.

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#### 177 Compressive Strength

The demoulded samples were left to rest at 20°C and a relative humidity of 75 % until the specific age of testing. The compressive strength of the prismatic sample fractured counterparts was tested after 1, 3, 7, 28 days in accordance with EN 196-1 using a universal testing machine (Instron 5960) at a constant loading rate of 144 kN/min. The compressive strength value was the average of values obtained from three specimens.

## 183 X-ray Diffraction (XRD) Analyses

The mineralogical compositions of the TMW and WG were obtained by powder X-ray diffraction (BRUKER D8 Advance) with an automatic slit, monochromated CuKα radiation ( $\lambda$ =1.5405 Å), 5-80° 2θ range, 0.600 s count time, Cu radiation, 40kV and 40mA. Peak shapes were studied using the program DIFFRACT.SUITE.

## 188 Fourier Transform Infra-Red (FTIR) Analyses

189 FTIR spectra were recorded from 400 to 4000 cm<sup>-1</sup> with a 2cm<sup>-1</sup> resolution, 5 kHz scanning

190 speed and 25 scan count using a Shimadzu IRAffinity-1 fitted with a Specac Quest attenuated

191 total reflectance (ATR) accessory.

#### 192 Scanning Electron Microscopy (SEM)

Microstructural studies utilised SEM (Zeiss Supra 35VP) equipped with EDS analyser (EDAX). Backscattered and Secondary electron images were collected from polished specimens to overcome the main limitation of fracture surfaces. To prepare the polished specimens, 5-mm-thick slices were cut using a low-speed saw. The samples were first impregnated with ultra-low viscosity resin and then polished.

#### 199 **Stopping the activation process**

200 Both the XRD and FTIR samples were tested in a state where the alkali activation process 201 was stopped using the combined water and solvent extraction protocol developed by Chen et 202 al. (2014). In summary, it involved stirring the AAB specimen in deionized water and then 203 removing the liquid by centrifuging. Upon addition of methanol, soluble silicate species 204 could be observed in the liquid layer. Thus water extraction by centrifuging was used to 205 remove the precipitates. Specimens were then ground to micron-sized particles using a mortar 206 and pestle, and a solvent of methanol/acetone mixture was added, followed by further grinding. The solvent was removed using vacuum filtration; this latter procedure was 207 208 repeated for five times.

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## 210 RESULTS AND DISCUSSION

#### 211 Influence of Waste Glass on Tungsten Mining Waste Reactivity

212 The recorded FTIR spectra of raw TMW and WG and blended as TMW/WG are shown in 213 Fig.2. For the spectra of WG, the highest absorption coefficient is associated with the Si-O bending vibration near 453 cm<sup>-1</sup>. A weaker band due to the bending mode near 1000 cm<sup>-1</sup> is 214 215 accompanied by the still weaker feature near 775 cm<sup>-1</sup>. For the TMW, the highest absorption coefficient is associated with the bending vibration of the Si-O between 465 and 424 cm<sup>-1</sup>. 216 Weaker features are associated with the bending vibration of Si-O at 984 cm<sup>-1</sup> and its 217 symmetric stretching vibration between 797 and 694 cm<sup>-1</sup>. The weakest bands at 827cm<sup>-1</sup> and 218 1163 cm<sup>-1</sup> can be associated with the bending of the Si-O bond of the original TMW. The 219 220 absorbance spectrum of the TMW/WG blend displays the same spectral bands as the raw 221 TMW, only at lower intensities, obviously due to the combination of different intensities.

222 Results of the XRD analyses shown in Fig.3 reveal that the TMW precursor material 223 predominantly consists of muscovite and silica with traces of sodium aluminosilicate,

rudashevskyite and pyrite and is similar to the TMW chemical composition identified by 224 225 Pacheco-Torgal et al. (2009). The WG is revealed to consist of silica, lime and sodium oxide 226 with traces of potassium and iron oxide. Using a general non-linear least squares system 227 software (TOPAS V5), the TMW and WG were determined to be 97% and 15% crystalline, 228 respectively. Compared to other materials commonly used as AAB precursors such as fly ash 229 (Van Jaarsveld and Van Deventer 1999) and metakaolin (Provis et al. 2005), the TMW is of a 230 far less amorphous nature. In this study, a sustainable approach was chosen to increase the 231 amorphicity of the TMW through the addition of WG. The addition of 40 wt.% WG led to an 232 increase in the amorphicity, qualitatively indicated by the more intense amorphous 233 background from 15° to 45° in the TMW/WG blend XRD spectrum and also by a 21% 234 calculated reduction in crystallinity. The compressive strength of TMW-WG AAB was used 235 to evaluate the strength contribution potential as a function of the degree of amorphicity. 236 Thus Fig.4 shows the evolution of compressive strength in TMW-WG AAB with 20, 30 and 237 40 wt.% WG replacement over 28 days. The results obtained for pure TMW AAB are also 238 included. Each reported result corresponds to the average measurement in three specimens 239 per each WG replacement value and age; the deviation of results fluctuated between 0.22 and 240 1.4%. In Fig.4 it can be observed the compressive strength increased with an increase in the 241 WG content at all ages. The highest 28-day strength was obtained by the 60TMW40WG 242 sample at 41MPa, which is 127% higher than the control sample 100TMW. The compressive 243 strength would be influenced primarily by the additional release of reactive silica. However, 244 it also expected that the CaO content in the WG would contribute to the strengthening of the 245 reaction products, most likely in the form of a (C, N)-A-S-H gel.

The compressive strength results with the highest replacement level of WG i.e. 40wt.% is consistent with the compressive strength results previously obtained by Pacheco-Torgal et al. (2009b), specifically 39.6 MPa at 28 days, for mortar prepared with TMW. However, this was achieved only after an energy intensive calcination treatment of the TMW at 950°C for 2
hours.

251 Finally, the reactive silica-containing WG combined with the highly alkaline activator 252 solution may create the potential for the deleterious process of alkali-silica reaction (ASR) 253 and required validation. TMW-WG AAB with the highest replacement of WG i.e. 40 wt.% 254 was stored at a RH of 80% at 38°C to accelerate the ASR reaction; a thin-section of this 255 sample shown in Fig.5. Observation of the section, which is representative of the WG as a 256 whole, revealed that there were no signs of ASR gel formation around the WG particles or in 257 the open voids. Data reported in the literature established that if the waste glass is ground 258 under 75 µm, the ASR effect does not occur, and binder durability is guaranteed (Shao et al. 259 2000b). Water is also a necessary condition for ASR; considering the TMW-WG AAB only required a water/precursor demand of 0.179, this may also be the reason for the absence of 260 ASR. 261

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## 263 Alkali Activator Preparation Conditions

264 To prepare the TMW-WG AAB, it is necessary that the alkali activator is in a homogeneous 265 state upon mixing with the powder precursors. Fig.6 shows the effect of activator mixing time on the 80TMW20WG AAB compressive strength. It can be seen that the 28-day strength 266 267 increases when using the activator which has been mixed between 2 and 5 minutes only (i.e. 268 M2.5 and M5), reaching the maximum 28-day strength of 17 MPa at an activator mixing time 269 of 5 minutes (i.e. M5). As the activator mixing time is extended, an immediate drop in 270 compressive strength is observed. The activator solution mixing time has a strong impact on 271 the 28-day strength, as a 26% drop in compressive strength is recorded for the TMW-WG 272 AAB when prepared using an activator solution stirred for 20 minutes i.e. M20. Fig.7 273 presents the results of the activator solution temperature during mixing. The black and red 274 curves represent the activator and enclosure air temperature, respectively. Over the course of 275 20 minutes of mixing, an average reduction of 3.13°C in activator temperature was recorded 276 from three identical tests, while the enclosure temperature was recorded to remain stable at 277 23°C±0.1°C. This drop activator solution temperature is an endothermic process resulting 278 from the reorientation of the water molecules, leading to a disruption of the hydration shells 279 surrounding the ions. The positive metal ions, in this case, Na<sup>+</sup>, are particularly at risk since 280 they inherently possess weaker attractions to the negative oxygen end of the water molecule. 281 The prolonged mixing can be thought to cause a net stripping effect of the water molecules 282 from the ions. The latter would impact the dissolution and subsequent mobility of the 283 siliceous material present in TMW and WG, leading to a less intense attack on the silicon-284 oxygen bonds and thus a reduction in mechanical performance, as verified by the results in 285 Fig.6.

286 Further interpretation of this is shown by the ATR-FTIR spectra of the activator mixed for 5 and 20 minutes in Fig.8. The 3270cm<sup>-1</sup> band (which is a sensitive and well-defined band 287 288 corresponding to the O-H vibrations in water) is revealed to increase in intensity by 21.4%, 289 which based on literature concerning FTIR spectra of water at different temperature 290 (Praprotnik et al. 2004), may be considered as a significant amount. It is an indication that the 291 activator solution mixed for 20 minutes possesses a higher unbound water content with fewer 292 solvated ions and more available as free molecules. Also, visually observed after 20 minutes 293 of mixing was the partial gelation of the soluble silicate anions detected by the loss of 294 uniform fluid flow and the adherence of solid gel to the glass wall. Polymerization of silicates 295 commonly occurs at pH close to neutral, but can also be triggered by an increased water 296 content (Hu et al. 1993). Gelation would also contribute to reducing the effectiveness of the 297 activator to balance the charge of the aluminate groups in the phyllosilicate, resulting in a 298 negative effect on the kinetics of the reaction and therefore the development of mechanical 299 strength. From a practical outlook, it must be emphasised that the preparation of the alkali

activator is independent of the mixing of the final binder. Therefore, the alkali-activators
dependence on mixing time should not be considered to interfere with the upscaling potential
of AABs.

## 303 TMW-WG AAB Curing Temperature and Curing Time

304 Samples T20 through to T80 in Table 2 were made so that the effect of different curing 305 temperatures on compressive strength of TMW-WG AAB could be studied. The prisms cast 306 were cured under sealed conditions at 20, 40, 60 and 80°C for 24h, then tested for compressive strength after 1, 3, 7 and 28 days. The compression strength results in Fig.9 307 308 present details on the role of temperature on the properties of TMW-WG AAB. The 309 compressive strength of all the samples at all ages increased with increasing curing 310 temperature. Samples cured at 20°C (i.e. T20) did not develop appreciable compressive 311 strength for the first 7 days of curing and were only able to attain 2.6 MPa after 28 days. The 312 highest compressive strengths were obtained by curing at 80°C (i.e. T80), allowing the 313 TMW-WG ABB to attain 22MPa at 28 days. From this, it can be concluded that the reaction 314 that took place was a temperature-driven process. Van Jaarsveld et al. (2002) and Bakharev 315 (2005) reported comparable compressive strength results for fly ash based AABs. Curing the 316 samples above 80°C was not attempted due to the sufficient strength gained from curing at 317 80°C. Higher temperatures would also require a greater energy input; a factor this study wanted to avoid by keeping the production of the binder as less energy intensive as 318 319 practically possible.

Fig.10 shows the FTIR spectra of the TMW/WG blend of raw materials and the TMW-WG AAB cured at different temperatures (i.e. T20-T80). The TMW-WG AAB cured at 20°C (i.e. T20), as expected, displays the highest absorbance, which can be inferred as reduced hardening activity and thus slow strength development. The spectra of samples cured at 40 324 and 60°C (i.e. T40 and T60) match each other closely indicating similar molecular structures 325 are present in both samples when curing at the respective temperatures. However, the change in absorbance for the sample cured at 80°C (i.e. T80) is more evident. The latter spectrum 326 shows a great reduction in absorbance and broadening between 850 and 1100 cm<sup>-1</sup> associated 327 328 with the Si-O-Si symmetric stretching vibrations for the gel product and is an indication of increased activation. A similar feature can be observed at 775 and 694 cm<sup>-1</sup>, the region of the 329 330 spectrum also representing symmetric stretching vibration of the raw material Si-O bonds. 331 The development of a more amorphous gel phase with the increase in curing temperature can 332 be inferred from the spectrum of the TMW-WG AAB sample at 80°C matching that of the 333 raw WG, which is confirmed to be inherently amorphous from the XRD results (refer to 334 Fig.3). Nonetheless, the presence of asymmetric stretching vibration (Si-O-Si) related to non-solubilised particles at ~1000 cm<sup>-1</sup> and ~450 cm<sup>-1</sup> in the TMW-WG AAB indicates that 335 336 unreacted precursor materials are still present, supporting the same result found in the XRD 337 analysis. Milling the precursor materials to a fine particle size has been shown to improve 338 reactivity and dissolution in an alkali activator solution. In the case of fly ash, Temuujin et al. 339 (2009) showed that vibration milling could reduce the median particle size by more than 50% 340 and improve the compressive strength by 80%. This method of mechanical activation could 341 potentially be used to improve the dissolution properties of TMW further, as long as the additional energy input did not compromise the low energy potential of the TMW-WG AAB. 342 343 Just as important as curing temperature is the AAB heat curing duration. Samples D4 through 344 to D36 in Table 2 were prepared to study the effect of curing time on the compressive 345 strength of TMW-WG AAB. Samples were cured in sealed conditions for 4, 12, 24 and 36h 346 at 80°C and tested for compressive strength after 1, 1.5 (36h), 3, 7 and 28 days. Fig.11 shows 347 that the compressive strength improves with an increase in curing time from 4 to 24h. The improvement in compressive strength continues at an even higher rate when the curing time 348

349 increases from 12 to 24h. However, after 36h of curing a depreciation of the compressive 350 strength at 36h (identified by the yellow marker in Fig.11), 3 days and 7 days is observed, 351 leaving the 28-day strength unchanged. Thus, it can be concluded that the activation reaction 352 that took place was time-dependent. Fig.12 shows the SEM images of TMW-WG AAB samples cured at 80°C for 24 and 36h. The microstructure of the sample cured for 24h 353 354 consists of close-packed quasi-unreacted WG particles embedded in a continuous matrix of gel products while the sample cured for 36h exhibits visible contraction, particularly around 355 356 the WG particles. Although samples were kept in sealed conditions during curing, it was 357 observed during de-moulding that some water was still able to evaporate into the surrounding 358 air within the curing bag. Previous work by Mo et al. (2014) suggested that the contraction of 359 AAB samples cured under sealed conditions at 80°C occurs after 7days. However, the results 360 of this study suggest that contraction can initiate as early as 36h. It is possible that prolonged 361 exposure to the elevated temperature may have led to the water evaporation rate being greater 362 than that of re-saturation, thus triggering the accumulation of internal stresses and subsequent 363 contraction of the AAB matrix.

364 The absorbance spectra for the raw TMW/WG blend and TMW-WG AAB, cured for varying periods of time (i.e. D4-D36) are shown in Fig.13. A reduction in the absorption intensity of 365 366 the main bands at ~1000, ~775 and ~446  $\text{cm}^{-1}$  indicates that longer curing times led to the further dissolution of Si-O from the raw materials. Also, the position of Si-O bending 367 368 vibration peaks shifted from 999 and 463 cm<sup>-1</sup> in the raw TMW/WG to 989 and 446 cm<sup>-1</sup> respectively for the TMW-WG AAB specimen cured for 24h, a type of shift associated with a 369 370 greater extent of polymerization in aluminosilicates (Sarkar et al. 2015). Also, it is important 371 to observe that the absorbance spectrum for the TMW-WG AAB sample cured for 24h (i.e. D24) displays lower absorbance intensities than the TMW-WG AAB sample cured for 36h. It 372 can be inferred from this latter result that curing times above 24h can lead a reduction in Si-O 373

dissolution and complements the mechanical strength results in Fig.11 which clearly show reductions in compressive strength for samples cured for 36h. Previous research regarding the curing time of AAB's made from fly ash (Li et al. 2013) and metakaolin (Heah et al. 2011) have uncovered similar results. Also, the broadening of the characteristic bands between 1100-850 cm<sup>-1</sup> and 800-750 cm<sup>-1</sup> implies the overlap of more bands with a higher intensity which in this case is attributed to the asymmetric stretching vibrations of T-O-Si (where T= Si or Al) (Khater 2013).

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## 382 CONCLUSIONS

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The effect of waste glass addition to tungsten mining waste alkali-activated binders was assessed by strength testing, XRD, SEM and FTIR. Additionally, preparation conditions such as activator mixing time, curing temperature and curing time on hardening kinetics was assessed, leading to the following discoveries:

The addition of WG is a very sustainable and practical method of improving TMW degree of amorphicity, compared to traditional calcination treatments. Up to 40 wt.%
 of WG with a mean particle size of 39.6µm can be successfully blended with TMW to increase the amorphous nature of the binary blend by 21%, without the initiation of the alkali-silica reaction.

Prolonged activator mixing can reduce the dissolution of the aluminosilicate precursor
 due to fewer available alkali metal ions in solution. The initiation of silicate gelation
 due to prolonged stirring would also contribute to reducing the activator effectiveness.
 The correct preparation of the activator solution is imperative and would be expected
 to extend to other classes of alkali activated cementitious systems.

The optimum conditions for obtaining the most significant dissolution of the alumino silicate oxides were curing for 80°C for 24h. When curing time is greater than 24h i.e.

36h as investigated in this study, it can lead to a reduction in compressive strength and

401 contraction of the AAB matrix, even under sealed conditions.

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Chemical compound	<b>TMW (%)</b>	TMW S.D	WG (%)
Na <sub>2</sub> O	1.31	1.45	9.72
MgO	1.01	2.98	0.00
Al <sub>2</sub> O <sub>3</sub>	21.06	2.53	0.00
SiO <sub>2</sub>	47.88	3.86	73.93
SO <sub>3</sub>	8.72	2.83	0.00
K <sub>2</sub> O	4.12	0.78	0.69
Fe <sub>2</sub> O <sub>3</sub>	9.97	2.73	0.40
P <sub>2</sub> O <sub>5</sub>	0.00	0.27	0.00
CaO	0.88	0.99	12.83
TiO <sub>2</sub>	0.66	0.35	0.00

**Table 1.** Chemical Composition (wt.%) of raw TMW, WG determined by SEM-EDX

Sample	Activator mixing time (mins)	Curing temperature (°C)	Oven curing duration(hours)
M2.5	2.5		
M5	5		
M10	10	60	24
M15	15		
M20	20		
T20	5	20	
T40		40	
T60		60	24
T80		80	
D4	5	80	4
D12			12
D24			24
D36			36

 Table 2. Summary of preparation and curing regimes for the variables studied

enclosure thermocouple



**Fig.1** SS/SH activator solution temperature measurement set up



575 wavenumber (cm<sup>-</sup>)
576 Fig.2 ATR-FTIR absorbance spectra of the as received raw TMW, WG, and TMW-WG
577 blend (80 and 20% mass fractions, respectively)





580 Fig.3 XRD patterns of TMW, WG and blended TMW/WG WG (1- silica, 2- muscovite, 3-

581 sodium aluminosilicate, 4- rudashevskyite, 5- pyrite)



**Fig.4** Effects of WG substitution on TMW AAB compressive strength



587 Fig.5 Polished thin-section of TMW-WG AAB with 40 wt.% WG at 28-days



590 Fig.6 Effect of SS/SH activator solution mixing time on 28-day compressive strength of

591 TMW-WG ABB cured at 60°C for 24 hours

592



**Fig.7** SS/SH activator solution temperature due to prolonged mixing



**Fig.8** ATR-FTIR spectrum of SS/SH activator solution with varying mixing time



**Fig.9** TMW-WG AAB compressive strength (1-28d), for samples cured for 24 h at 20, 40, 60

601 and 80°C.



**Fig.10** ATR-FTIR absorbance spectra of as received raw TMW/WG and TMW-WG AAB at

- 28 days cured at 40, 60 and 80  $^{\circ}\mathrm{C}$ 



607

608 Fig.11 TMW-WG AAB compressive strength (1-28d), for samples cured at 80°C for 4, 12,

- 609 24 and 36 h.
- 610



- 612 Fig.12 TMW-WG ABB sample cured at  $80^{\circ}$ C for (a) 24 h and (b) 36 h



**Fig.13** ATR-FTIR absorbance spectra of as received raw TMW/WG and TMW-WG AAB at

616 28 days cured at 80°C for 4, 12, 24 and 36 h.