

32 structure-soil interaction in engineering [2], robotics locomotion [3,4], and the astrophysical
33 realm[5]. In addition, intruder penetration in immersed granular media is also ubiquitous in
34 multiple realms, such as soil bed erosion by saturated debris flows [6], penetration tests in marine
35 beds [7] and underwater crater formation in geological fields [8]. This process offers valuable
36 insights into granular behavior, as it occurs in different stages where the substrate media exhibits
37 characteristics of both solids and fluids. This suggests that granular media undergoes phase
38 transitions, determined by its mechanical behavior, as it transitions between different flow regimes
39 [9].

40 Considerable research efforts have been dedicated to understanding the mechanism of
41 penetration in granular materials. In the quasi-static regime, the resistance encountered during
42 penetration is similar to that of a regular fluid [10,11], and the modified Archimedean law has been
43 used for predictions [12,13]. However, beyond the quasi-static regime, the proportionality of the
44 force F_z to the depth z alone is insufficient. An additional term F_v proportional to the square of the
45 velocity v , representing the inertial effect, is introduced [14-19]. In these cases, the resulting
46 resistance can be estimated by $F(z, v) = F_z(z) + F_v(v^2)$ when the $v > v_c = \sqrt{2gd_g}$, with v_c
47 being the speed of a particle falling under gravity [17]. While the separate contributions of depth
48 and velocity to the drag force are widely discussed in the context of impact processes [14,20,21],
49 the underlying physical justification remains unclear due to the interplay between depth and
50 velocity during the dynamic events. This complexity is further amplified in the immersed case,
51 where the response of the fluid-solid mixture substrate becomes intricate. Consequently, previous
52 investigations on this problem are via either a continuum or discrete approach [9,16,22-28].
53 However, the isolated mechanisms governing the $F_z(z)$ and $F_v(v^2)$ terms are yet to be fully
54 elucidated. Recent studies [29,30] have shed light on the distinct nature of the $F_v(v^2)$ term, which
55 deviates from theoretical expectations. Nevertheless, a comprehensive understanding of the
56 settlement behavior of granular materials, including momentum transfer and local or nonlocal
57 rheology evidence, remains incomplete, particularly in the context of the immersed case. Here, we
58 try to reveal the underlying mechanism of drag force both in the dry and immersed cases,
59 meanwhile uncovering the analogy and correlation between the two scenarios.

60

61 **Model description and numerical setup**

62 To investigate the coupling mechanisms between velocity (v) and depth (z) and to examine the
63 influence of the ambient fluid, this study aimed to establish a general numerical approach for
64 understanding the intrusion phenomena. A coupled computational fluid dynamics and discrete
65 element method (CFD-DEM) implemented in the software PFC 3D (Particle Flow Code) and
66 OpenFOAM model was employed to simulate the impact penetration process at a constant velocity
67 (v_0). Unlike previous approaches using homogenized the particles and fluid, the current model
68 explicitly solved the individual motion of particles and fluid [28]. In this study, polydispersed
69 grains were utilized to mimic natural granular packing state and prevent crystallization. The rolling
70 resistance contact model, accounting for angular particle shapes, was incorporated to capture the
71 shape effect [31]. In the immersed case, the fluid and particle motion were derived from the
72 numerical solution of the Navier-Stokes equations and the second Newtonian law, respectively,
73 using a coarse-grid coupled scheme [32].

74 The simulation setup is depicted in Figure 1(a-b). A frictional spherical intruder with a
75 diameter (D) of 2.2 cm ($6.1d_g$, d_g = mean grain diameter) and a density of 7.8 g/cm^3 was initially
76 placed at the bed surface and then forced to penetrate into a granular bed at a constant speed (v_0)
77 ranging from 25 cm/s to 500 cm/s. The bed container dimensions were sufficiently large ($W/D >$
78 10) to minimize boundary effects, following the size recommendations adopted in the experimental
79 and numerical investigations [29,33]. This configuration also enables the simultaneous capture of
80 both the quasi-static and inertial regimes. The granular bed consisted of grains with a diameter (d_g)
81 in the range of $3.6 \pm 1.8 \text{ mm}$, as shown in Figure 1(a), with a density (ρ_g) of 2.6 g/cm^3 . The particle
82 interactions were governed by a contact model developed based on physical principles where the
83 contact behavior among the normal, shear, rolling, and twisting directions has been related by the
84 integration algorithms in the finite contact area, incorporating parameters such as the effective
85 contact modulus ($E = 7 \times 10^7 \text{ Pa}$), shape parameter ($\beta = 0.25$), local crushing coefficient ($\xi_c = 4.0$),
86 and friction coefficient ($\mu = 0.5$), the further detail could be found in the Supplemental Material
87 [34]. The granular sample was prepared using the under-compaction multi-layer method (UCM)
88 [35] and consolidated under the influence of gravity ($g = 9.8 \text{ m/s}^2$). The resulting granular volume
89 packing fraction (ϕ) was 0.61, indicating a dilatation required for flow and the emergence of the
90 breakage of jamming states during the penetration [18,36]. The time step is auto-calibrated by the
91 software during the simulation as $1e^{-6} \text{ s}$ according to the contact stiffness and particle mass,
92 meanwhile kinematic constraints are applied. In the immersed case, the mesh size is selected as

93 the same as the intruder. Water properties were set for the fluid, with a density (ρ_f) of 1000 kg/m^3
 94 and a kinetic viscosity (ν) of $10^{-6} \text{ m}^2/\text{s}$. The time step of fluid is set as $1e^{-4} \text{ s}$ fitting the CFL
 95 condition, which leads to the exchange frequency equal to 100. Additional detailed information
 96 regarding the numerical method and model setup can be found in the Supplementary Material [34].

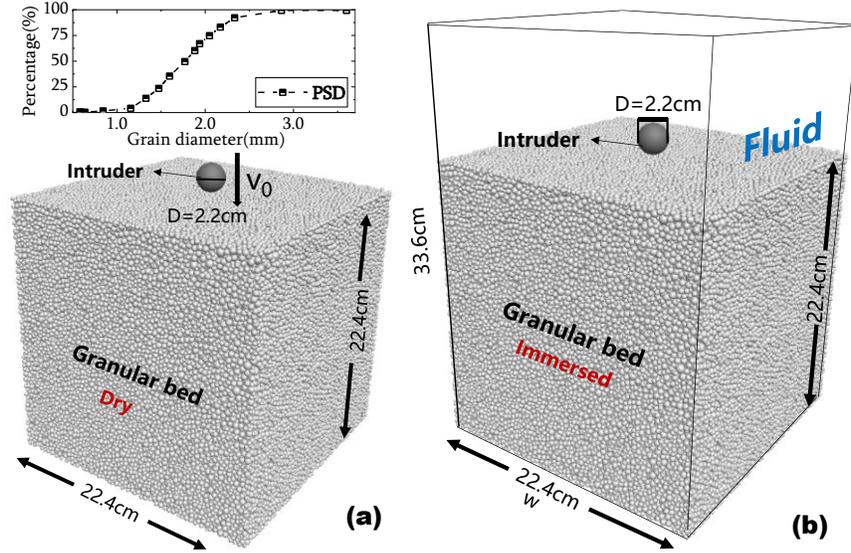


FIG. 1. (a) Particle size distribution (PSD) of polydispersed grains and the numerical model configuration of the dry modelling scenario; (b) numerical model configuration of the immersed modelling scenario.

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98 Results and discussion

99 A. Drag force evolution

100 Figure 2(a) displays the evolution of the drag force $F(z, v_0)$ with the dimensionless penetration
 101 depth $\tilde{z}=z/D$ (normalized by the intruder size) in both the dry and immersed modelling scenarios,
 102 recalling the complete phenomenon observed in previous studies [29,37]. Through a
 103 comprehensive analysis of the drag force F , important insights are gained. Contrary to the expected
 104 $F(z, v) = F_z(z) + F_v(v^2)$ relationship depicted in the inset plot of Figure 2(b), both the dry and
 105 immersed cases exhibit distinct trends to reach the depth-dependence stage. As indicated in Figure
 106 2(a)-(b), the beginning of the penetration process (referred to as the initial contact stage) exhibits
 107 velocity dependence. A sharp peak, denoted as the peak force (F_{peak}), occurs at $\tilde{z}\sim 0.25$, similar to
 108 what has been reported in the impact process ($\tilde{z}\sim 0.125$). Subsequently, during the transition stage,
 109 fluctuations of varying magnitudes are observed in distinct scenarios (dry and immersed),
 110 suggesting the reorganization of the granular medium following intense perturbations [29,30].

111 Eventually, all $F(z, v_0)$ curves, with different v_0 values, converge into the same increasing slope
 112 $dF/d\tilde{z}$ in the dry case (referred to as the depth-dependence stage). In contrast, in the immersed case,
 113 though in the depth-dependence stage, the $dF/d\tilde{z}$ is still positively correlated to the penetration
 114 velocity. The depth at which the stage transition from ‘transition’ to ‘depth-dependence’ occurs is
 115 defined as the characteristic depth (z^*) and the corresponding F value is referred to as the
 116 characteristic force (F^*). The ambient fluid affected the penetration process by attenuating the
 117 fluctuations and increasing the magnitude level of the drag force F . This effect is evident in the
 118 larger characteristic force F^* and the subsequent higher $dF/d\tilde{z}$ values in the depth-dependence
 119 stage of the immersed case.

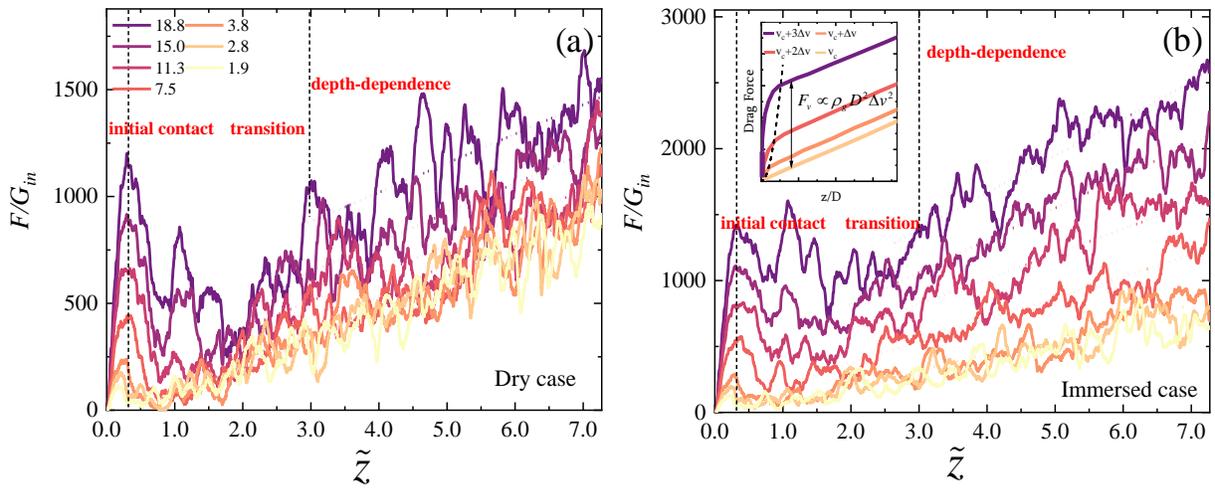


FIG. 2. The drag force offered by granular bulk on a spherical intruder versus z in different speeds in (a) dry and (b) immersed modelling scenarios, respectively. The vertical dashed lines delimit the stages and the inclined dashed lines are the linear fitting. The inset plot in (b): Expected results from the theoretical model, Δv : the incremental penetration velocity of the intruder. The drag force is normalized by the weight of the intruder $G_{in} = m_{in}g$ and the penetration velocity is normalized by the $v_c = \sqrt{2gd_g}$.

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121 B. Regime identification

122 The distinct intrusion characteristics, including the peak force F_{peak} , characteristic force F^* , and
 123 characteristic depth z^* , have been examined in detail to provide a comprehensive description of
 124 the different stages. Figure 3(a) presents the scaling law between the peak force F_{peak} and
 125 penetration velocity v_0 . Interestingly, the linear correlation observed in both the immersed and dry
 126 cases contradicts previous findings [29] of a quadratic dependence. However, this linear
 127 relationship between F_{peak} and v_0 aligns with experimental results related to drag force in plow or

128 upward drag problems [36,38]. This deviation from the previously observed quadratic dependence
129 can be attributed to the break-up of the jamming state, during which the granular bulk transitions
130 from a static state to a flow regime [39,40]. The dilatancy characteristic of granular material, which
131 was accounted for in this study through rolling and twisting resistances, may contribute to the more
132 intense shear-dilatancy behavior in the dense state. The inset plot in Figure 3(a) demonstrates the
133 gradual convergence of F/v_0 versus \tilde{z} evolution trend, indicating the velocity-dependence
134 characteristic with distinct ‘viscous’ behavior in this stage. As shown in Figure 2(b), the quadratic
135 scaling law between F^* and v_0 is observed in both the immersed and dry modelling scenarios and
136 imply the ‘inertial effect’, albeit with different fitting coefficients. Meanwhile similar convergence
137 trend of F/v_0^2 in different ranges of penetration depth can be observed in the inset plot, which
138 indicates the collisional momentum transfer [30]. The observed difference in F^* caused by the
139 ambient fluid in the transition stage indeed deviates from the initial stage which is with a slight
140 difference in F_{peak} caused by the interstitial fluid. This evidence suggests different action
141 mechanisms of fluid in these two different stages (i.e. initial contact, transition). The relationship
142 between z^* and v_0 , depicted in Figure 3(c), illustrates the characteristic of dynamic relaxation for
143 the granular bulk during intrusion. The negligible difference between the two cases indicates that
144 the ambient fluid does not affect the intrusion depth required for particle contact network
145 reorganization [41]. Recall the inset plot of Figure 3(b), the consistency between the depth at which
146 F/v_0^2 deviates from the overlapping collapse trend and the corresponding z^* is obtained. This
147 observation indicates the progression towards depth-dependence stage (quasi-static regime) is
148 accompanied by a gradual reduction in the inertial effect, as evidenced by the quadratic velocity
149 dependency relationship.

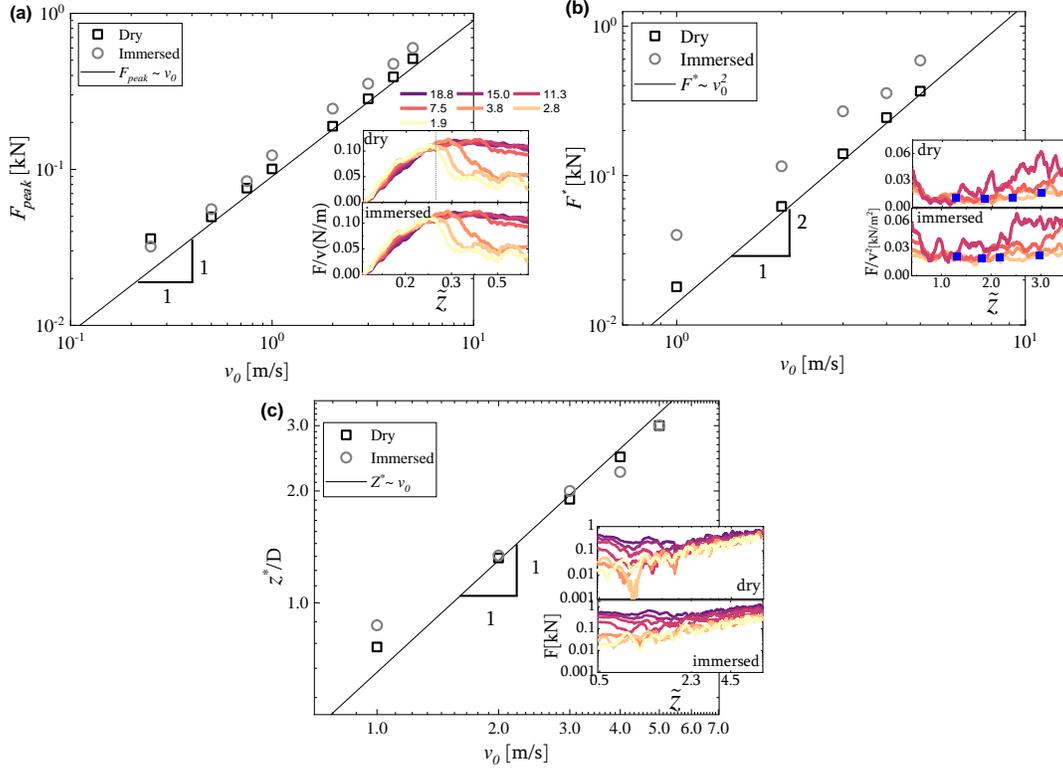


FIG. 3. (a) Correlation between peak force F_{peak} and penetration velocity v_0 . The inset plot is the drag force scaled by the velocity as the function of the penetration depth \tilde{z} . (b) Correlation between the characteristic force F^* and penetration velocity v_0 . The inset plot is the drag force scaled by the quadratic velocity as the function of the depth \tilde{z} , and the separation time is marked as solid blue squares. (c) Correlation between the characteristic depth z^* and the penetration velocity v_0 . The inset plot is the log-log relationship between the drag force F and penetration depth \tilde{z} . In (b)(c), the data points corresponding to the intruder velocity less than 1 m/s were ignored due to their weak inertial effect.

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Filtering the fluctuations provided by the discrete characteristic of granular media, Fig. 4 presents a schematic extracted trend of the penetration process to reflect the main feature of the drag force evolution, which captures the essential characteristics of the initial contact, transition, and depth-dependence stage. The state curves for the linear $F \sim \tilde{z}$ and quadratic $F \sim \tilde{z}^2$ functions define the boundaries of different stages. Furthermore, the underlying quasi-static and inertial regimes of these stages are also highlighted. In the inset plot of Fig. 4(a), the experimental and numerical data from previous studies [30,42] are summarized, demonstrating the same power law with different coefficients that confirm the generality of the observed behavior. Despite

159 quantitative deviations, the immersed case follows a similar regime hierarchy to the dry case. A
 160 comparison with the ideal pattern of the drag force's evolution shown in the inset of Fig. 2(b)
 161 suggests a shared underlying physical nature, while highlighting the different approaches to the
 162 depth-dependence regime. The theoretical model neglects the state transformation from the
 163 jamming state [39,43] in the initial contact stage and the progressive evolution of compound
 164 components ($F_z(z)$, $F_v(v)$, and $F_v(v^2)$) in the transition stage, presents a more idealized
 165 inheritance mechanism of the inertial effect.

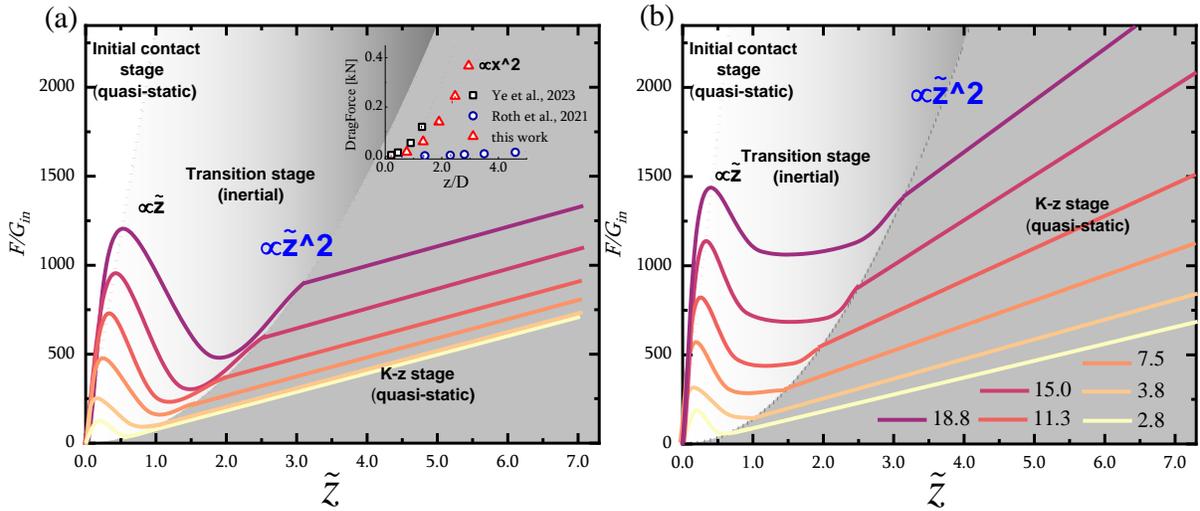


Fig 4 (a) The relationship between $F \sim \tilde{z}$ derived from the numerical results. The delimitation line is marked as the dashed line. The inset plot summarizes the published numerical and experimental results [30,42]. (b) the extracted model adapted to the immersed case. The drag force is normalized by the weight of the intruder $G_{in} = m_{in}g$ and the penetration velocity is normalized by the $v_c = \sqrt{2gd_g}$.

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167 C. Local measurements

168 For the mechanical analysis, the local rheology measurement [44] is employed to provide a
 169 comprehensive understanding of the effect of the ambient fluid and the underlying mechanisms
 170 governing dry and immersed granular materials. The variable protocol begins with the
 171 decomposition of the strain rate and stress tensor, denoted as $\dot{\epsilon}$ and σ , into isotropic and deviatoric
 172 parts: $\dot{\epsilon} = \dot{\epsilon} \mathbf{I} + \dot{\epsilon}_d$ and $\sigma = -p \mathbf{I} + \sigma_d$. Here, \mathbf{I} represents the unit tensor; $\dot{\epsilon} = \frac{1}{3} \text{tr}(\dot{\epsilon}) = \frac{1}{3} \text{div } \mathbf{v}$ is
 173 the dilation rate; $\dot{\epsilon}_d$ is the shear rate tensor; p is the pressure; and σ_d is the shear stress tensor.
 174 Scalar quantities corresponding to the invariants of the strain rate and stress tensors are presented,
 175 including the dilation rate, pressure, shear rate ($\dot{\gamma}$), and shear stress (τ). Further detailed calculation

176 approaches of the physical field could be found in the Supplementary Material [34]. The analysis
 177 focuses on an intermediate penetration velocity (v_0) of 3.0 m/s, chosen to reveal detailed
 178 mechanisms. Two measurement circles of the same size as and moving together with the intruder
 179 (characteristic length) are selected: the central area directly beneath the intruder and the direct edge
 180 next to the intruder at the same vertical position. The spatially averaged approach has been adopted
 181 to the lateral monitoring point. As a result, these monitored areas provide insights into the local
 182 flow characteristics surrounding the intruder.

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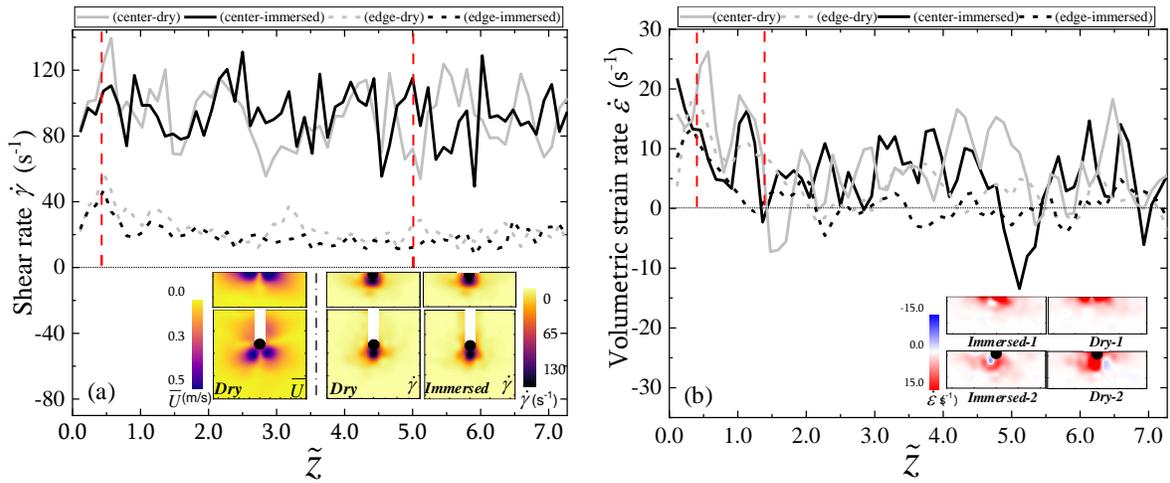


Fig 5 (a)-(b) the evolution of the shear rate $\dot{\gamma}$ and dilation rate $\dot{\epsilon}$ versus penetration depth \tilde{z} in different regions. The boundary between the dilation and contraction is marked as the horizontal black dashed line in (b). The inset plot is the field distribution of the corresponding properties extracted from the position marked by the vertical red dashed line.

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185 The evolutions of the shear rate ($\dot{\gamma}$) and dilation rate ($\dot{\epsilon}$) are presented in Fig 5(a) and (b),
 186 respectively, while the time-averaged quantities are summarized in Table 1. Throughout the
 187 penetration process, $\dot{\gamma}$ remains almost constant, with larger values observed in the central area. On
 188 the other hand, $\dot{\epsilon}$ reaches a stable state once the intruder is fully submerged, with higher values
 189 observed in the central area, consistent with $\dot{\gamma}$. The spatial distribution of the relevant physical
 190 value is illustrated in the inset plots. From the plot of averaged velocity \bar{U} , the symmetric pattern
 191 with the stagnant area underneath the intruder was observed, similar to the findings presented in
 192 the experiment [45]. The shear-rate contour shows the coincident results as the curves of the main
 193 plot that the highest shear rate emerges underneath the intruder. The similar shear-rate evolution

194 pattern between the different depths discussed here is reflected by the stable state mentioned before.
 195 As for the volumetric strain rate in the inset plot, the large fluctuations characteristic and the spatial
 196 distribution feature could be verified qualitatively. Based on the time-averaged results in Table 1,
 197 the effect of the ambient fluid on the strain rate ($\dot{\epsilon}$) is identified. The interstitial fluid enhances the
 198 shear-dilation behavior in both the edge and central areas, while it has no effect on $\dot{\gamma}$. It can be
 199 speculated that this effect of the ambient fluid on the strain rate has a synergistic mechanism with
 200 the increased pressure observed in the immersed bulk granular media. This suggests a potential
 201 rheological explanation for the influence of the fluid based on the higher pressure in the immersed
 202 case.

Table 1 Time-average results of strain-rate

	$\langle \dot{\gamma} \rangle (\text{s}^{-1})$				$\langle \dot{\epsilon} \rangle (\text{s}^{-1})$	
	Edge	Center		Edge	Center	
Immersed	19.075	93.064	Immersed	1.358	5.621	
Dry	21.121	92.380	Dry	3.860	7.531	

203
 204 The evolution of stress (including pressure and shear stress) in the central and edge areas
 205 is shown in Fig 6(a) and (b), respectively. The significant differences between these two locations
 206 indicate the localization of stress beneath the intruder and the emergence of higher stress in the
 207 immersed case, providing a mesoscale explanation for the influence of the ambient fluid on the
 208 macroscopic drag force. Furthermore, the consistent evolution patterns between shear stress (τ),
 209 pressure (p), and drag force (F in Fig. 2) suggest that the resistance is determined by the integration
 210 of stress applied to the interface. From the contour, the concentrated stress appears in the bottom
 211 area of the intruder meanwhile the larger stress level in the immersed case could also be
 212 distinguished from the pattern feature.

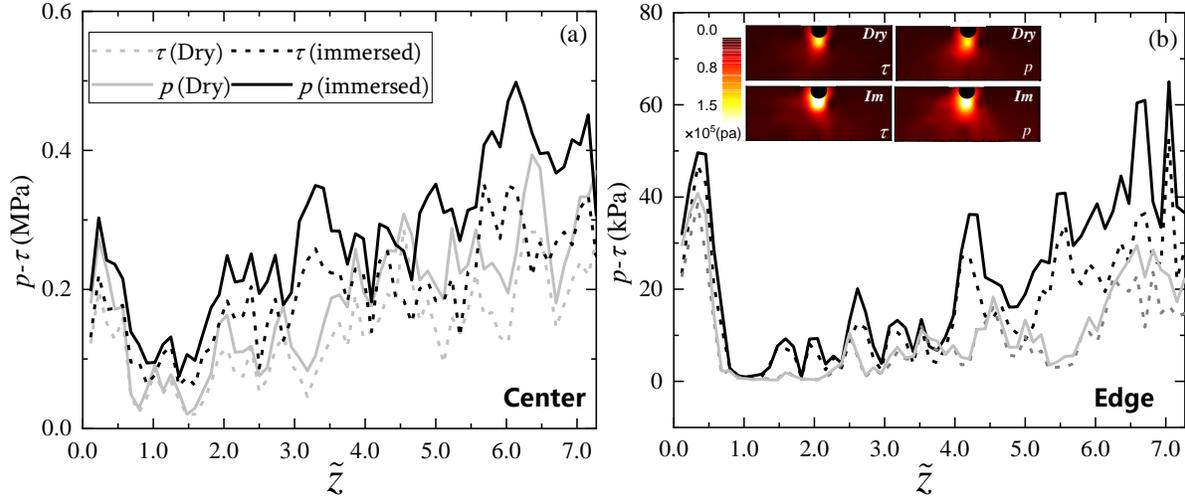


Fig 6 (a)-(b) the evolution of the shear stress (τ) and pressure (p) versus penetration depth \tilde{Z} in different regions. The inset plot in (b) is the corresponding field distribution extracted from the position marked by the vertical red dashed line and the symbol is on the plot.

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As one of the key granular properties, the granular temperature T has been considered to essentially affect the origin of the non-local behavior [46]. It could be defined as the mean square of the fluctuations of the particle velocity as $T = \langle (v - \langle v \rangle)^2 \rangle$ [47], where $\langle \dots \rangle$ computes the spatial averaged value. It can be further normalized as $T^* = T\rho/p$, where the p is the pressure. Fig 7 illustrates the variation of T^* and T in regions beneath and surrounding the intruder during the penetration process. The dimensionless temperature exhibits a rapid increasing trend in the transition stage which indicates the inertial granular flow. In addition, combined with the same evolution pattern of the inertial number, it could be derived that the T^* monitored is correlated to the inertial number as pointed out in the literature [47]. Regarding the spatial distribution feature, the granular material in the lateral position indicates a high inertial state with intense velocity fluctuations. As shown in the inset plot, after the initial contact stage, the non-dimensional granular temperature exhibits a nearly steady state, which is similar to the time evolution of the shear rate, and subsequently, this consistency states the strong correlation between the two variables. As a result, a stronger kinetic behavior has been observed in the lateral regions near the intruder both in the dry and immersed modelling scenarios. In the underneath region, the low temperature T^* is observed. The comparison indicates that the ambient fluid has a certain weakening impact on the dimensionless temperature, which originates from the constrained effect provided by the viscous interaction.

232 It needs to be noted that the granular temperature is related to the non-local behavior
 233 through the ‘diffuse’ process and induces ‘creep’ motion and destruction at some positions with
 234 relatively lower energy. The ‘cooling’ effect provided by the ambient fluid originates from the
 235 constraints of the particles’ kinetic behavior, which has potentially changed the non-local behavior
 236 by decreasing the temperature gradient. However, this topic is beyond the scope of this work and
 237 could be investigated in future work.
 238

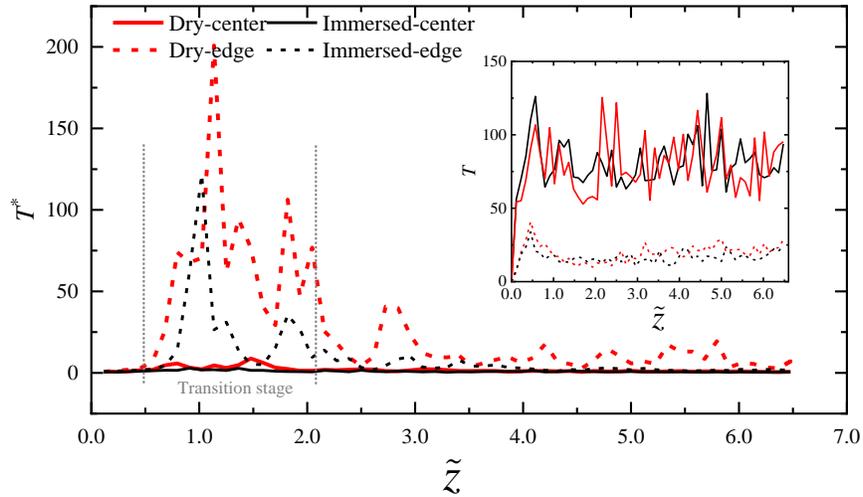


Fig 7. The dimensionless granular temperature (T^*) versus normalized depth(\tilde{z})in regions beneath and surrounding the intruder for the dry and immersed modelling scenarios. The inset plot shows the evolution of the granular temperature (T).

239

240 **D. Rheological mechanism**

241 The rheological characteristics of the granular media under the influence of the intruder are
 242 depicted in Fig 8, for the effective friction coefficient $\mu = \tau/p$, viscosity $\eta = \tau/\dot{\gamma}$, and the inertial
 243 number $I = |\dot{\gamma}|d/(P/\rho_s)^{0.5}$. The inertial number I provides comprehensive insights and aids in
 244 determining the granular flow regime, which is closely related to other granular properties
 245 mentioned in previous sections. In Fig 8(a), the inertial number I increases sharply at the intruder
 246 impact, and peaks quickly in the transition stage. The value of I in the region surrounding the
 247 intruder surpasses the inertial effect limit and eventually returns to the quasi-static state. During
 248 this process, the ambient fluid could significantly influence the flow regime of the granular bulk,
 249 where the momentum transfer between the fluid and particles slows down the granular flow

250 dynamics through the viscous effect. As shown in the inset plot of Fig 8(a), the contour of the
 251 effective friction coefficient is demonstrated in the transition stage to reflect the correlation
 252 between μ and I in spatial distribution. It could be observed that the peak values emerge near the
 253 intruder, indicating the main agitated flowing region there. The comparative results of the contour
 254 between the immersed and dry cases are consistent with the evolution of inertial number. In the
 255 transition stage, the immersed granular materials present lower value of μ which is expected by
 256 the low inertial values illustrated by the main plot. In Fig 8(b), the time evolution of the viscosity
 257 is plotted, as contrary to the trend of inertial number I , the viscosity undergoes the descending and
 258 then recovering trend in the transition stage. The inset plot illustrates the spatial distribution of
 259 viscosity, in which the agitated region during the penetration process can be clearly identified. The
 260 observed peak value underneath the intruder of the immersed scenario indicates the low inertial
 261 region among the granular bed. Furthermore, the ambient fluid strengthened viscosity during the
 262 penetration process, resulting in a higher resistant force, especially with nearly the same shear rate
 263 as shown in Table 1.

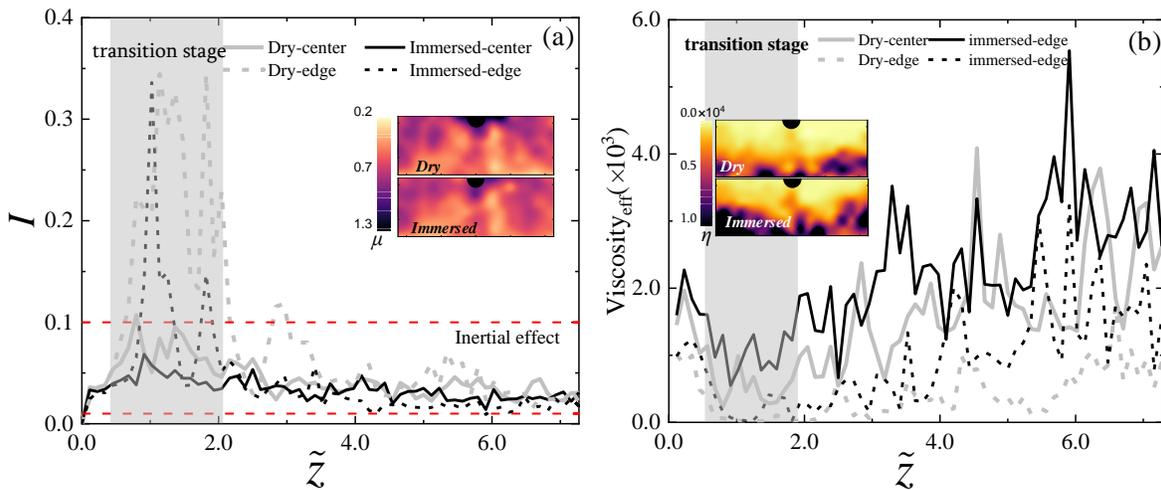


Fig 8. The evolution of the inertial number I (a) and the viscosity η (b) during the penetration process in the different regions(center, edge). The inset plots are the contour of the effective friction μ (in (a)) and η (in (b)) in the transition stage.

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265 As shown in Fig 9(a), the parameters I and μ are non-linearly positively correlated, which
 266 aligns with the classical local rheology model $\mu(I) = \mu_s + (\mu_2 - \mu_s)/(I_0/I + 1)$ [48]
 267 qualitatively in both the immersed and dry cases. In Fig 9(b), the viscosity η and inertial number I
 268 follows a $\eta \sim I^{-2}$ scaling law. For the granular material, the transition of mechanical responses is

269 always accompanied by the evolution of the granular structures, including the texture and the
 270 lifespan characteristic of the contact force. In line with the observed phenomenon, the
 271 corresponding structural evolution in the granular bulk during the penetration is revealed and
 272 interpreted by the coordination number C_n in Fig 9(c). A clear $C_n \sim I^{-1}$ scaling law between C_n and
 273 I is observed indicating a decreasing contact in the intensely flowing materials, which is consistent
 274 with the results reported in the literature [49]. Combining the evolution of I in Fig 8(a), it can be
 275 observed that after the initial contact stage with a relatively intact contact net, the region
 276 surrounding the intruder experiences intense fluidization, with some regions displaying extremely
 277 low coordination numbers. This indicates a complete suspension state wherein the collision
 278 becomes dominant. Finally, the C_n recovers in the depth-dependence stage, indicating the
 279 recurrence of the quasi-static regime. This analysis unveils the micro reflection of the inertial
 280 number I at the grain scale.

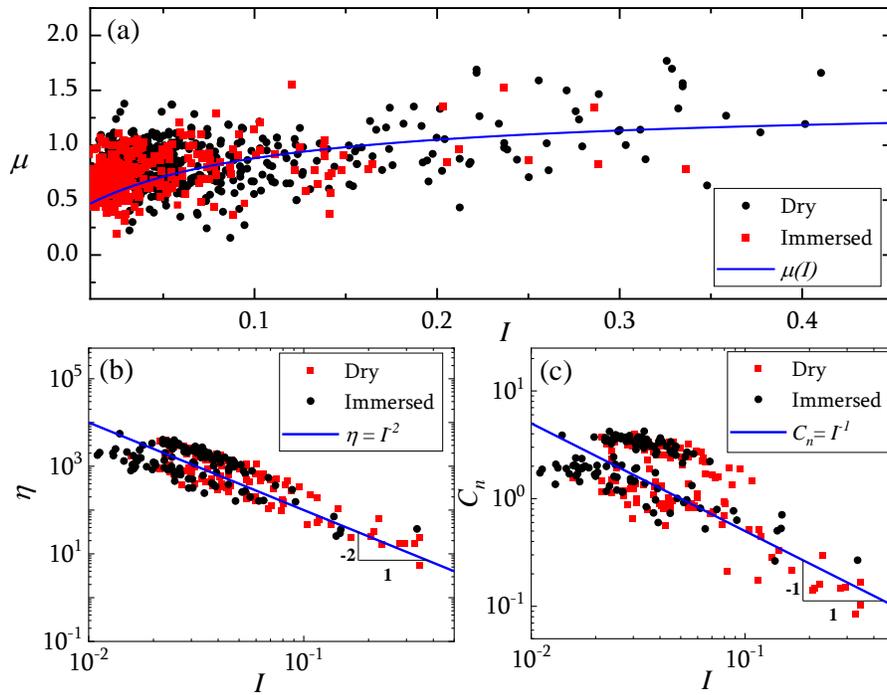


FIG 9.(a): The relationship between the I and μ , where the fitting curve (blue line) is the function $\mu(I) = \mu_s + (\mu_2 - \mu_s)/(I_0/I + 1)$. (b) - (c): the relationship between the viscosity η , coordination number C_n , and inertial number I

281
 282 During the penetration, the ambient fluid restrains the flow dynamics of the granular material,
 283 specifically in the low inertial regime. However, it seems that the same rheological characteristic

284 is shared between the dry and immersed cases, as illustrated in Fig 9(a). In essence, the
285 combination of high η and low I led to the low dynamics of penetration stage for a $F \sim v_0$ relationship,
286 while the combination of low η and high I facilitated the $F \sim v_0^2$ relationship for high penetration
287 dynamics. This observation also reflects the decisive role of the Reynolds number Re_p in the drag
288 force of Newtonian fluids for a gradually transition from laminar flow to turbulent flow as Re_p
289 increases. These findings inspire a homology between I and Re_p in the granular intrusion process.
290 It needs to be noted that the numerical simulations conducted in this research manifest the ‘Fluid-
291 inertial’ regime according to the regime phase from the literature [50]. Therefore, the expected
292 unified rheology of the $\mu - I$ correlation between the dry and immersed cases was observed, which
293 has further validated our work. Meanwhile, the mechanism of penetration in the ‘viscous’ regime
294 will be the next stage in the path approach to the complete unified theory/description.

295

296 **Conclusions**

297 The constant penetration in the granular bulk, both in the dry and immersed modelling scenarios,
298 has been studied using a coupled numerical simulation model. Through the local rheology
299 measurement, the dynamics of the drag force and its underlying mechanisms were explored.
300 Various regimes were observed in the system, including the initial contact stage with $F_{peak} \sim v_0$
301 relationship, signifying the viscous behavior, followed by the transition stage characterized by
302 fluidization and viscosity reduction. The depth-dependence regime showed a viscosity and inertial
303 state recovery, and the proposed $F \sim \bar{z}^2$ line aligned well with some existing published work. The
304 evolution of local flow characteristics has been checked and the influence of the ambient fluid was
305 investigated, revealing its constraining effect on granular flow dynamics, resulting in a lower
306 inertial number I and granular temperature T^* . Nonlinear correlations in $\mu(I)$, $\eta(I)$, and $C_n(I)$ were
307 evaluated and validated in both dry and immersed cases, indicating that the same rheology
308 properties were shared by both scenarios. By disentangling velocity and depth-dependent
309 contributions to the drag force, a general drag force evolution pattern unifying dry and immersed
310 cases was proposed, which captures the common features ($F_{peak} = F(v)$, $z^* = F(v)$, and $F^* = F(v^2)$)
311 and state the distinct mechanism from multi-scale perspective. Overall, The study provided new
312 insights into the rheological mechanism in the penetration process for both dry and immersed
313 granular material, and the unified characteristics of this phenomenon.

314

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323

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